

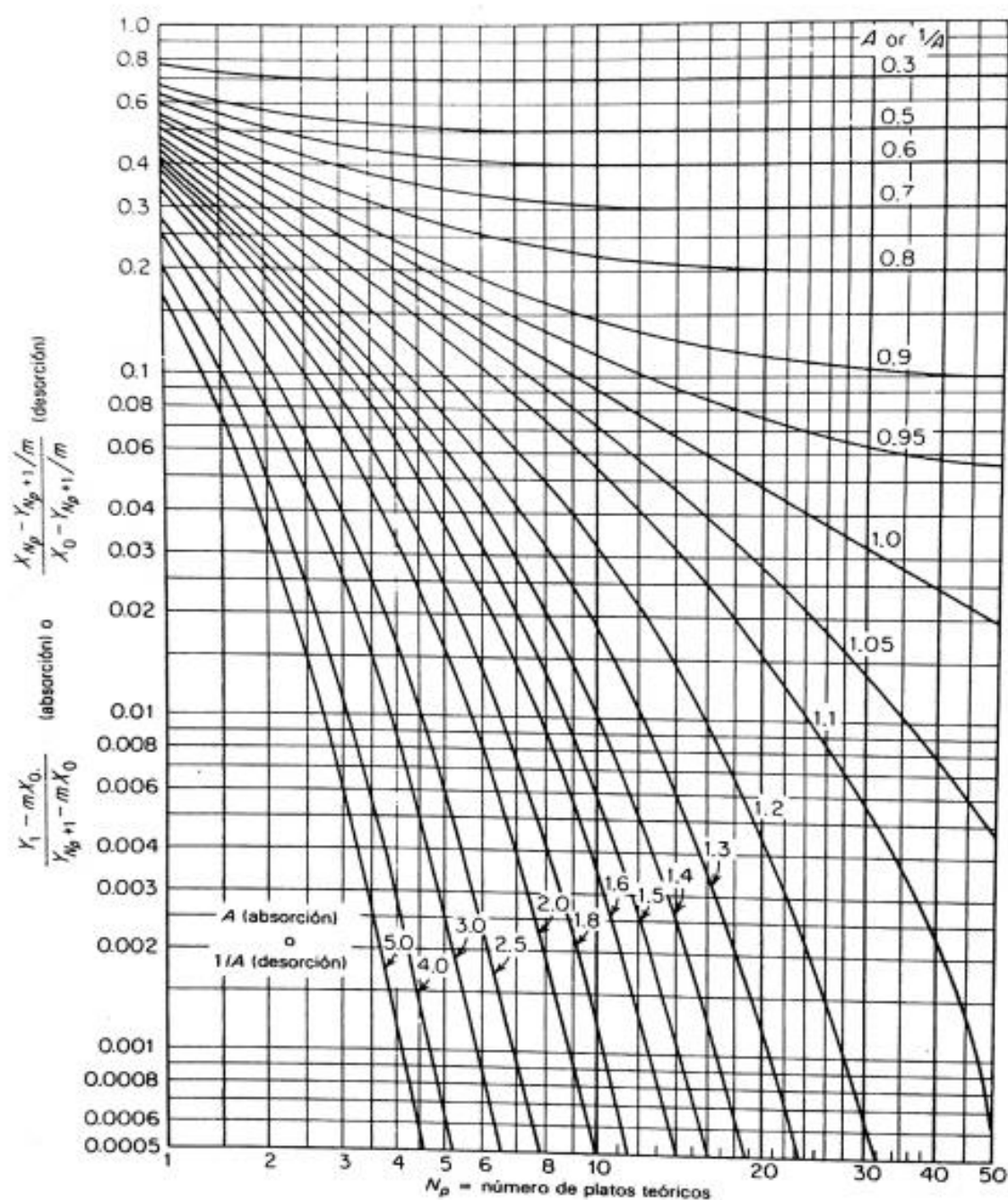


Figura 5.16 Número de etapas teóricas para cascadas a contracorriente, con el equilibrio de la Ley de Henry y factores de absorción o desorción constantes. [Por Hachmuth y Vance, *chem. Eng. Progr.*, 48, 523, 570, 617 (1952)].

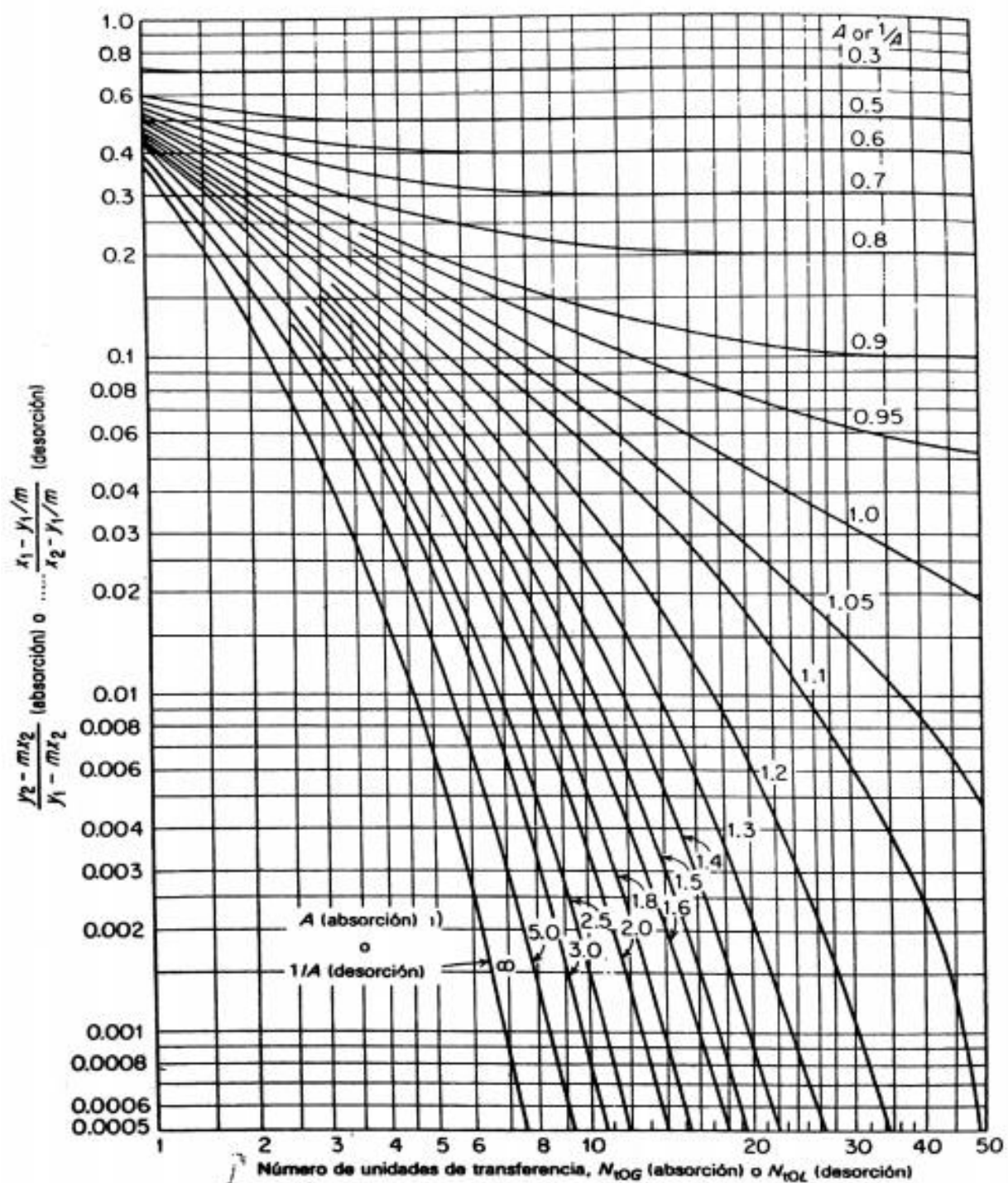


Figura 8.20 Número de unidades de transferencia para absorbedores o desorbedores con factor de absorción o desorción constante.

EQUIPMENT FOR DISTILLATION, GAS ABSORPTION, PHASE DISPERSION, AND PHASE SEPARATION

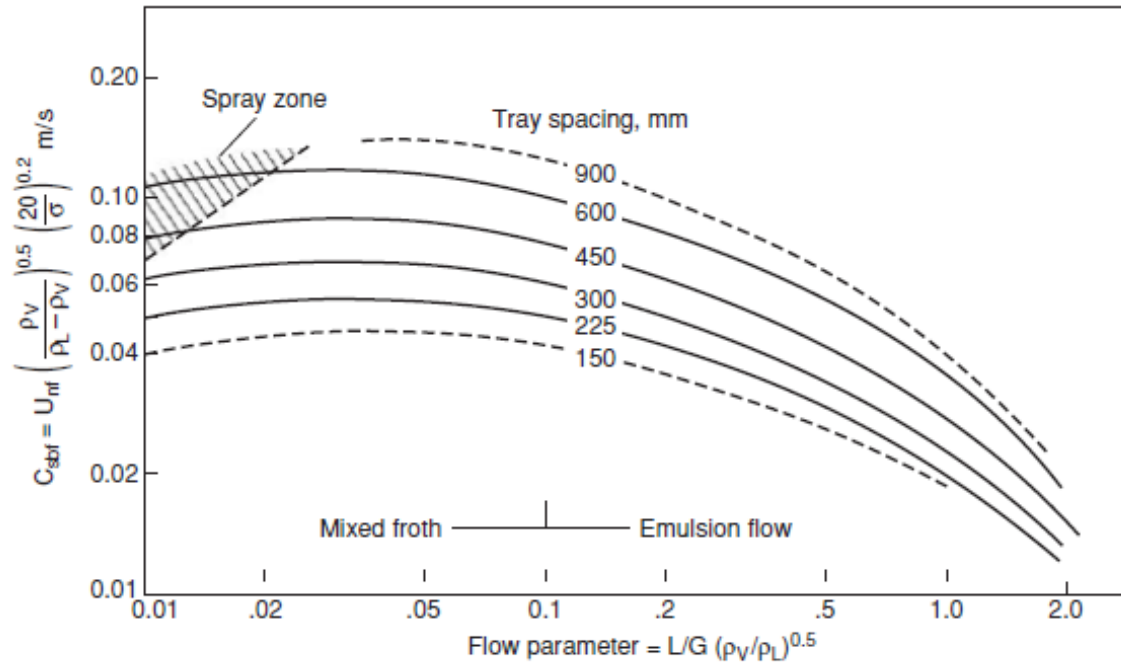
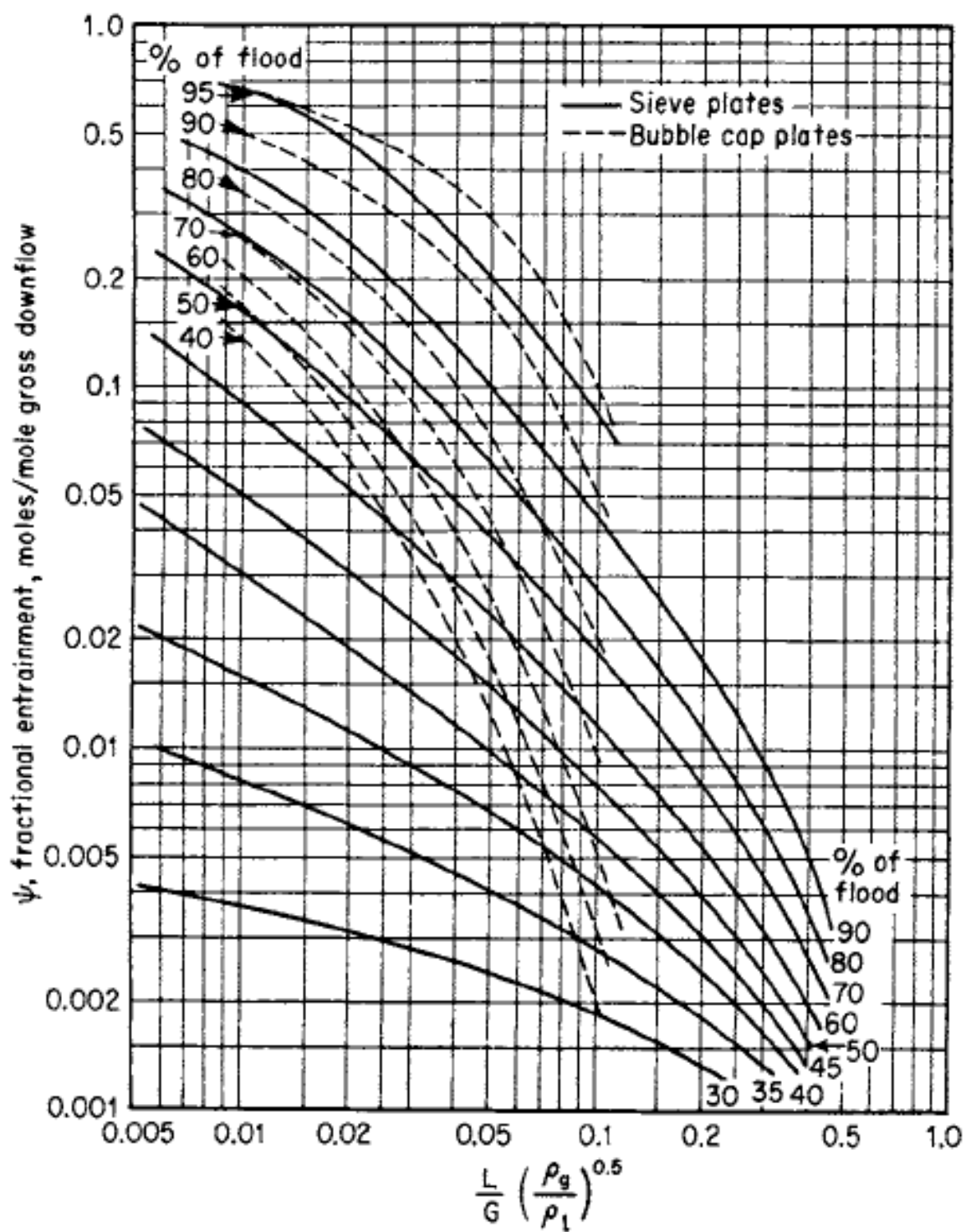


FIG. 14-31 Fair's entrainment flooding correlation for columns with crossflow trays (sieve, valve, bubble-cap). [Fair, *Pet/Chem Eng* 33(10), 45 (September 1961).]



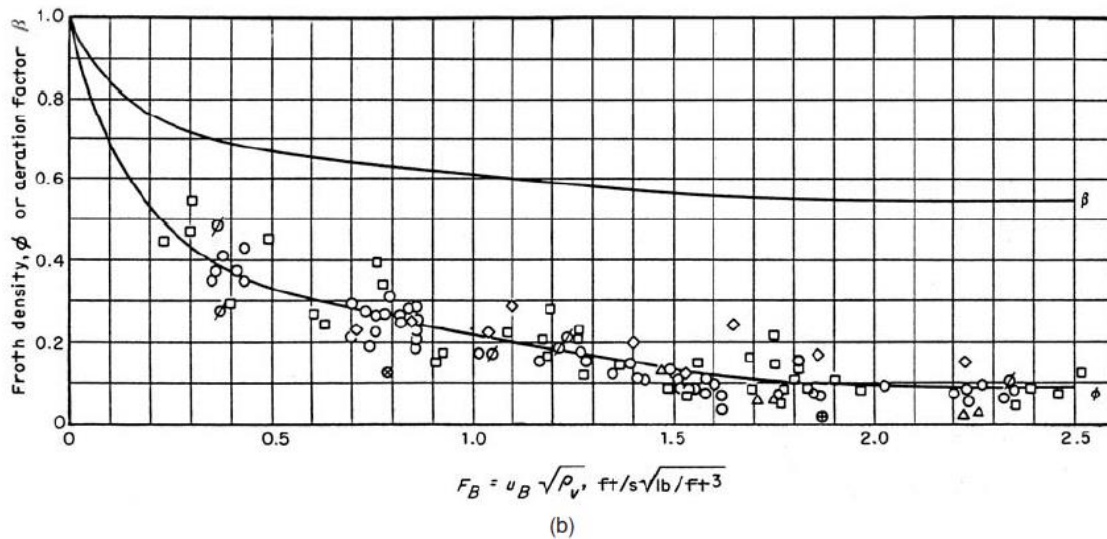
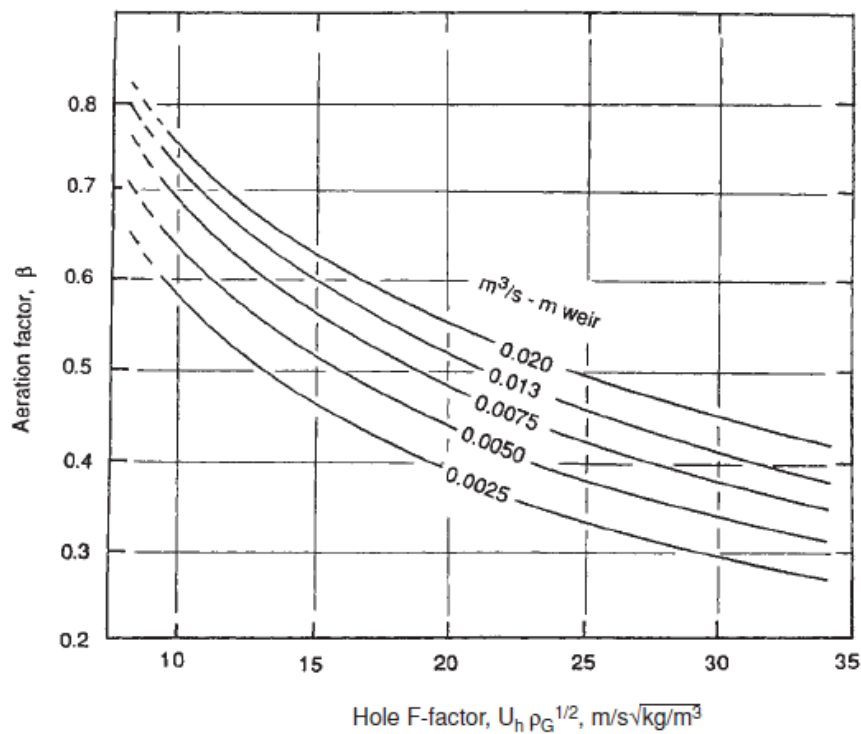


FIG. 14-37 Aeration factor for pressure drop calculation. (a) Sieve trays. [Bolles and Fair, Encyclopedia of Chemical Processing and Design, vols. 16, 86, J. M. McKetta (ed.), Marcel Dekker, New York, 1982.] (b) Valve trays. (From G. F. Klein, Chem. Eng., May 3, 1982, p. 81; reprinted courtesy of Chemical Engineering.)

EQUIPMENT FOR DISTILLATION AND GAS ABSORPTION: TRAY COLUMNS



EQUIPMENT FOR DISTILLATION, GAS ABSORPTION, PHASE DISPERSION, AND PHASE SEPARATION

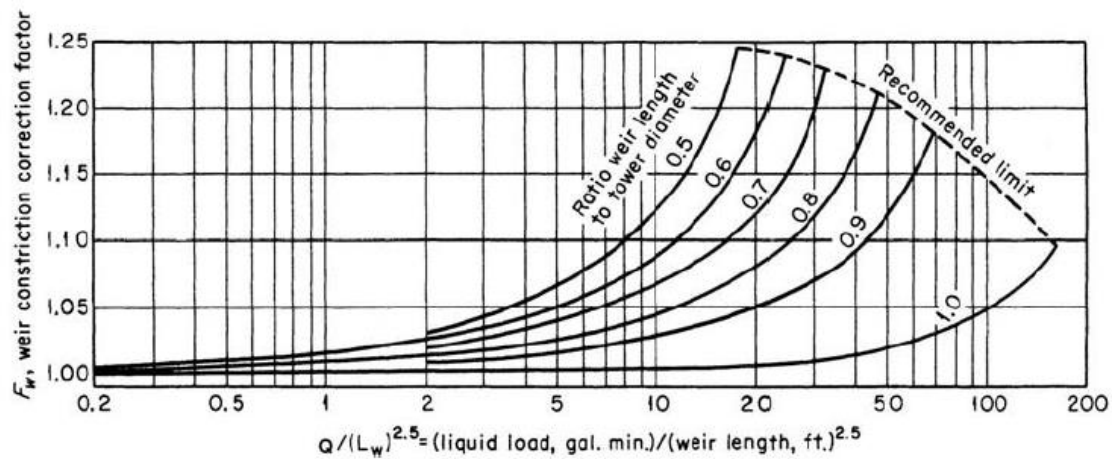


FIG. 14-38 Correction for effective weir length. To convert gallons per minute to cubic meters per second, multiply by 6.309×10^{-5} ; to convert feet to meters, multiply by 0.3048. [Bolles, *Pet. Refiner*, **25**, 613 (1946).]

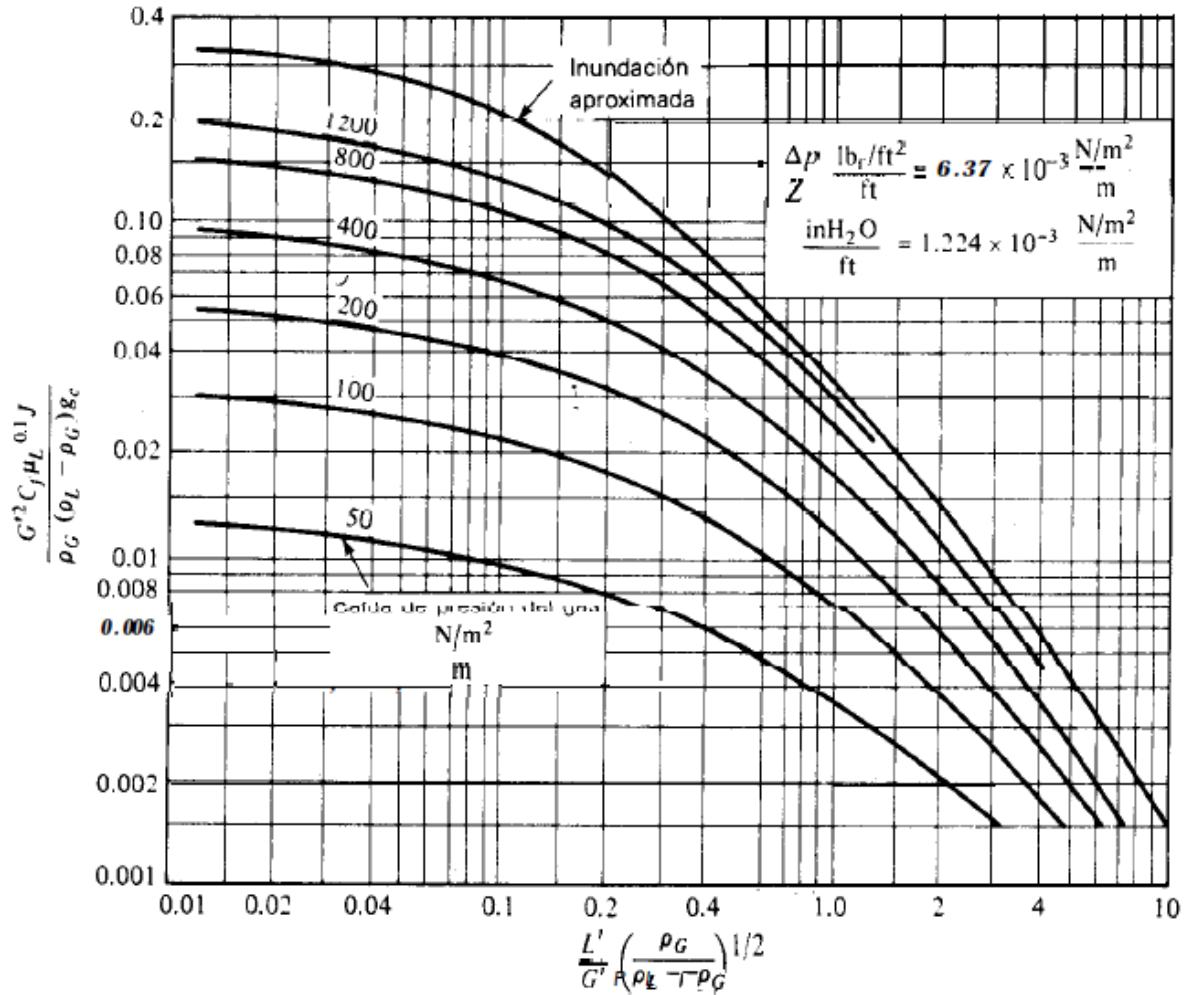


Figura 6.34 Inundación y caída de presión en torres con empaques al azar (coordenadas de Eckert [37], *Chemical Process Products Division, Norton Co.*) Para unidades SI (kg, m, s), $g_c = 1$, C_f de la tabla 6.3, y utilizar $J = 1$. Para $G^2 = \text{lb}_m/\text{ft}^2 \cdot \text{h}$, $\rho = \text{lb}_m/\text{ft}^3$, $\mu_L = \text{centip.}$, $g_c = 4.18(10^8)$, C_f de la tabla 6.3, y utilizar $J = 1.502$.

Tabla 6.3 Características de los empaques **aleatorios**^a

Empaque	Tamaño nominal, mm (in)										89 (3½)
	6 (¼)	9.5 (¾)	13 (½)	16 (⅝)	19 (¾)	25 (1)	32 (1¼)	38 (1½)	50 (2)	76 (3)	
	Anillos de Raschig										
Cerámica:											
Espesor de pared, mm	0.8	1.6	2.4	2.4	2.4	3	4.8	4.8	6	9.5	
C_f	1600	1000	580	380	255	155	125	95	65	37	
C_D			909	749	457	301		181.8	135.6		
ϵ	0.73	0.68	0.63	0.68	0.73	0.73	0.74	0.71	0.74	0.78	
$q_p, m^2/m^3 (ft^2/ft^3)$	787 (240)	508 (155)	364 (111)	328 (100)	262 (80)	190 (58)	148 (45)	125 (38)	92 (28)	62 (19)	
Metal											
0.8 mm pared											
C_f	700	390	300	170	155	115					
ϵ	0.69		0.84		0.88	0.92					
$q_p, m^2/m^3 (ft^2/ft^3)$	774 (236)		420 (128)		274 (83.5)	206 (62.7)					
1.6 mm pared											
C_f			410	290	220	137	110	83	57	32	
C_D			688	431	485	304		172.9	133.5		
ϵ			0.73		0.78	0.85	0.87	0.90	0.92	0.95	
$q_p, m^2/m^3 (ft^2/ft^3)$			387 (118)		236 (71.8)	186 (56.7)	162 (49.3)	135 (41.2)	103 (31.4)	68 (20.6)	

Anillos de Pall

Plástico									
C_f			97		52		40	25	16
CD			207		105.2		61.8	47.5	23.9
ϵ			0.87		0.90		0.91	0.92	0.92
$q_p, \text{m}^2/\text{m}^3 (\text{ft}^2/\text{ft}^3)$			341 (104)		206 (63)		128 (39)	102 (31)	85 (26)
Metal									
C_f			70		48		28	20	16
CD			133.4		95.5		56.6	36.5	
ϵ			0.93		0.94		0.95	0.96	
$q_p, \text{m}^2/\text{m}^3 (\text{ft}^2/\text{ft}^3)$			341 (104)		206 (63)		128 (39)	102 (31)	
Flexirings									
C_f			78		45		28	22	18
ϵ			0.92		0.94		0.96	0.96	0.97
$q_p, \text{m}^2/\text{m}^3 (\text{ft}^2/\text{ft}^3)$			345 (105)		213 (65)		131 (40)	115 (35)	92 (28)
Hy-pak:†									
C_f					45			18	15
CD					88.1			28.1	26.6
ϵ					0.96			0.97	0.97

Tabla 6.3 Continuación

Packing	Tamaño nominal, mm (in)										
	6 ($\frac{1}{4}$)	9.5 ($\frac{3}{8}$)	13 ($\frac{1}{2}$)	16 ($\frac{5}{8}$)	19 ($\frac{3}{4}$)	25 (1)	32 ($1\frac{1}{4}$)	38 ($1\frac{1}{2}$)	50 (2)	76 (3)	89 ($3\frac{1}{2}$)
Sillas de montar de Berl											
Cerámica	900		240		170	110		65	45		
C_f			508		295	184					
C_D			0.63		0.66	0.69		0.75	0.72		
ϵ	0.60										
$a_p, m^2/m^3 (ft^2/ft^3)$	899 (274)		466 (142)		269 (82)	249 (76)		144 (44)	105 (32)		
Sillas Intalox											
Cerámica	725	330	200		145	98		52	40	22	
C_f			399		256	241.5		36.2	71.3	40.6	
C_D			0.78		0.77	0.775		3.81	0.79		
ϵ	0.75										
$a_p, m^2/m^3 (ft^2/ft^3)$	984 (300)		623 (190)		335 (102)	256 (78)		195 (59.5)	118 (36)		
Plástico											
C_f						33			21	16	
C_D						96.7			56.5	30.1	
ϵ						0.91			0.93	0.94	
$a_p, m^2/m^3 (ft^2/ft^3)$						207 (63)			108 (33)	89 (27)	
SuperIntalox											
Cerámica ^c						60			30		
C_f						123			63.3		
C_D						0.79			0.81		
ϵ											
$a_p, m^2/m^3 (ft^2/ft^3)$						253 (77)			105 (32)		
Plástico ^d											
C_f						33			21	16	
C_D						79.5			53.5	30.1	
ϵ						0.90			0.93	0.94	
$a_p, m^2/m^3 (ft^2/ft^3)$						207 (63)			108 (33)	89 (27)	
Tellerettes											
Plástico										67-mm	95-mm (R)
C_f						40			20		
ϵ						0.87			0.93	0.93	0.92
$a_p, m^2/m^3 (ft^2/ft^3)$						180 (55)			112 (34)	112 (34)	

^a Los datos son para el empaque arrojado húmedo. Cortesía: Chemical Process Products Division, Norton Co.; Koch Engineering Co.; Ceilcote Co.; Chemical Engineering Progress; Chemical Engineer.

^b Tamaño nominal y espesor de la pared, mm, resp.: 6, 0.8; 9.5, 1.6; 13 a 19, 2.4; 25, 3; 32 y 38, 4.8; 50, 6; 76, 9.5.

^c a_p en $m^2/m^3 (ft^2/ft^3)$

^d Tamaños 1, 2 y 3